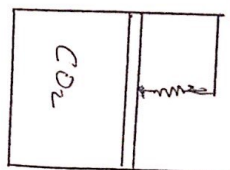


The shown sketch contains two kg of Carbon dioxide, which is heated from 100 kPa and 25°C to 1000 kPa and 300°C. Sketch the PV diagram and find the heat added.



$$m = 2 \text{ kg}$$

$$P_1 = 100 \text{ kPa}$$

$$T_1 = 25 + 273$$

$$P_2 = 1000 \text{ kPa}$$

$$T_2 = 300 + 273$$

$$C_v = 0.657 \text{ kJ/kg}\cdot\text{K}$$

$$C_p = 0.846 \text{ kJ/kg}\cdot\text{K}$$

$$w = \frac{(P_1 + P_2)(V_2 - V_1)}{2}$$

$$w = 550 \text{ J}$$

$$w = 500.5 \text{ kJ}$$

$$Q = w + \Delta E$$

$$Q - w = \Delta E$$

$$\Delta u = C_v(T_2 - T_1)$$

$$= 0.657(275)$$

$$\text{Sol: } R = 0.1889$$

$$P_1 V_1 = m R T_1$$

$$V_1 = \frac{m R T_1}{P_1}$$

$$V_1 = \frac{2(0.1889)(298)}{100}$$

$$100$$

$$V_1 = 1.128 \text{ m}^3$$

$$V_1 = \frac{V}{m} \Rightarrow 0.563 \text{ m}^3/\text{kg} = V_1$$

$$V_2 = \frac{m R T_2}{P_2}$$

$$P_2$$

$$V_2 = \frac{2(0.1889)(573)}{1000}$$

$$1000$$

$$V_2 = 0.2166 \text{ m}^3$$

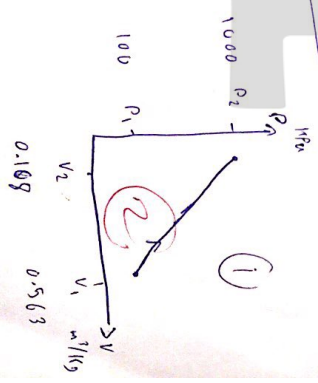
$$V_2 = \frac{V}{m} \Rightarrow 0.108 \text{ m}^3/\text{kg} = V_2$$

$$h = C_p \Delta T$$

$$h = 0.846(573 - 298)$$

$$h = 232.65 \text{ kJ/kg}$$

→ heat added



2. The shown arrangement contains 1 kg of water at 150 C and 100 kPa. How much heat must be removed to condense 50% of the steam. Given the piston diameter to be 1 m and it is initially 1.5 m above the stops. Also sketch the PV diagram

H₂O

~~m~~
m = 1 kg

T = 150 C

P₁ = 100 kPa

d = 1 m

State 3:

The volume will be constant

$$V_2 = V_3 = 1.1781$$

$$V_3 = \cancel{V_2} = \cancel{0.96835 \text{ m}^3/\text{kg}}$$

P = 200 kPa

So $W_b = 0$

$$W_b = P(V_2 - V_1)(m) = 100(1.1781 - 1.9367)(1)$$

$$W = -75.86 \text{ kJ}$$

$$u_2 = u_f + x u_{fg} = 417.4 + (0.695)(2088.2) = 1868.7 \text{ kJ/kg}$$

Soln: at state 1

The phase is superheated

$$V_1 = 1.9367 \text{ m}^3/\text{kg}$$

$$u_1 = 2582.9 \text{ kJ/kg}$$

$$h_1 = 2776.6$$

$$Q = W + m(u_2 - u_1)$$

$$= -75.86 + (1)(1868.7 - 2582.9)$$

$$Q = -790.06 \text{ kJ} \rightarrow \text{heat must be removed}$$

$$V_2 = \frac{1}{2} V_1$$

$$V_2 = 0.96835 \text{ m}^3/\text{kg}$$

State 2

$$V = xA$$

$$= (1.5) \left(\frac{\pi}{4} 1^2 \right)$$

no for stop

Assume the phase

$$\frac{V}{m} = 1.1781 \text{ m}^3/\text{kg}$$

wet mixture

at P = 100 kPa because it's free volume

$$T_2 = 99.61 \text{ } / V_f = 0.001043 / V_g = 1.6941$$

$$V_{ov} = V_f + x V_{fg}$$

$$1.1781$$

$$x = \frac{1.1781 - 0.001043}{1.6941 - 0.001043}$$

$$1.893057$$

$$x = 0.695$$

so it's wet mixture

$$x = 0.695$$

$x = 0.5$
↑ given

