



UNIVERSITY OF JORDAN  
SCHOOL OF ENGINEERING  
MECHANICAL ENGINEERING DEPARTMENT

جامعة  
الأردنية

Course Name: Thermodynamic II

Course No.: 0904342

Instructor: Eng.Rebhi AlMashaleh

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Reg. No.: 0147182

Serial No.:

Section No. 1

**Directions:** This is a 70 Minutes, Open-book and closed-notes examination. You are expected to do your own work. Your mobile must be turned off and you have to deliver it before your entrance to the exam hall.

**Grading Scheme**

Question	Question Grade	Student Grade
1	10	<u>8.5</u>
2	12	<u>11</u>
3	8	<u>8</u>
<b>Total Score</b>	<b>30</b>	$\Sigma =$ <u>27.5</u>

# Problem 1: (10 marks) Multiple Answer Questions

1. The Carnot cycle cannot be realized in practice, the reason being that

- (A) The pump work is very large
- (B) The heat addition cannot be accomplished at constant temperature
- (C) Both of the mentioned
- (D) None of the above

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2. Rankine cycle efficiency of a good steam power plant may be in the range of

- (A) 15 to 20%
- (B) 35 to 45%
- (C) 70 to 80%
- (D) 90 to 95%

3. The cycle that after partial expansion in turbine, steam is brought back to boiler is called

- (A) Reheating cycle
- (B) Regeneration cycle
- (C) Cogeneration cycle
- (D) Combined cycle

4. The actual work in the turbine and pump compared to isentropic ones are

- (A) Both Greater than the isentropic ones
- (B) Both Less than the isentropic ones
- (C) For pump less but for turbine greater
- (D) For turbine less but for pump greater

5. The undesirable effect when increasing the boiler pressure can be corrected by

- (A) Reheating the steam
- (B) Adding vacuum pump
- (C) Regenerating the steam
- (D) Superheating the steam

6. An Open FWH regenerative is basically

- (A) Direct mixing of the steam and feed water
- (B) Indirect mixing of steam and feed water in a heat exchanger
- (C) Both of the mentioned
- (D) None of the above

7. If we increase the superheat at constant pressure then the cycle efficiency

- (A) Decrease, increases
- (B) Increase, decreases
- (C) Increase, increases
- (D) Decrease, decreases

8. To prevent erosion of blades in turbine, quality should not fall below

- (A) 85%
- (B) 90%
- (C) 95%
- (D) 100%

9. The efficiency of regenerative cycle is greater than that of the Rankine cycle since

- (A) The mean temperature of heat addition increases
- (B) The mean temperature of heat addition decreases
- (C) The pump work decreases
- (D) None of the mentioned

10. The correct sequence of expansion in a reheat cycle is

- (A) HP turbine – LP turbine – constant pressure in boiler
- (B) HP turbine – constant pressure in boiler – LP turbine
- (C) LP turbine – constant pressure in boiler – HP turbine
- (D) LP turbine – HP turbine – constant pressure in boiler

**1. The compressor in refrigeration cycle is used to**

- (A) Raise the pressure of the refrigerant
- (B) Raise the temperature of the refrigerant
- (C) Circulate the refrigerant through the refrigeration cycle
- (D) All of the above

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**2. One ton of the refrigeration is**

- (A) The standard unit used in refrigeration problems
- (B) The cooling effect produced by melting 1 ton of ice
- (C) The refrigeration effect to freeze 1 ton of water at  $0^{\circ}\text{C}$  into ice at  $0^{\circ}\text{C}$  in 24 hours
- (D) The refrigeration effect to produce 1 ton of ice at NTP conditions

**3. Freon group of refrigerants are**

- (A) Chlorofluorocarbons (B) Hydrofluorocarbons (C) Ammonia (D) carbon dioxide

**4. For obtaining high COP, the pressure range of compressor should be**

- (A) High
- (B) Low
- (C) Optimum
- (D) Any value

**5. In a refrigeration system, the expansion device is connected between the**

- (A) Compressor and condenser
- (B) Condenser and receiver
- (C) Receiver and evaporator
- (D) Evaporator and compressor

**6. The refrigerant for a refrigerator cycle should have**

- (A) Minimum mass flow rate
- (B) Low boiling point
- (C) High enthalpy of vaporization
- (D) All of the above

**7. The COP increases sharply with evaporator temperature increase, particularly:**

- (A) At high condensing temperatures
- (B) At low condensing temperatures
- (C) At high compressor work
- (D) None of the above

**8. The major drawback of ammonia which makes it unsuitable for domestic use is**

- (A) Its toxicity (B) Its high cost (C) Its low boiling point (D) Its effect on the ozone layer

**9. The major problem associated with Air-source heat pump is:**

- (A) The frost accumulation on the evaporator coils
- (B) Its lower COP
- (C) Its expensive cost
- (D) Its effect on the ozone layer

**10. Cascade refrigeration cycle used in case of**

- (A) Large pressure range in the cycle
- (B) Poor performance for a reciprocating compressor
- (C) Low temperature applications required
- (D) All of the above

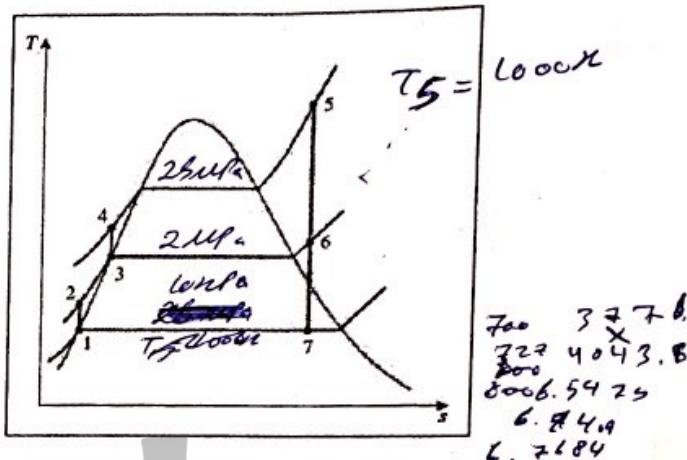
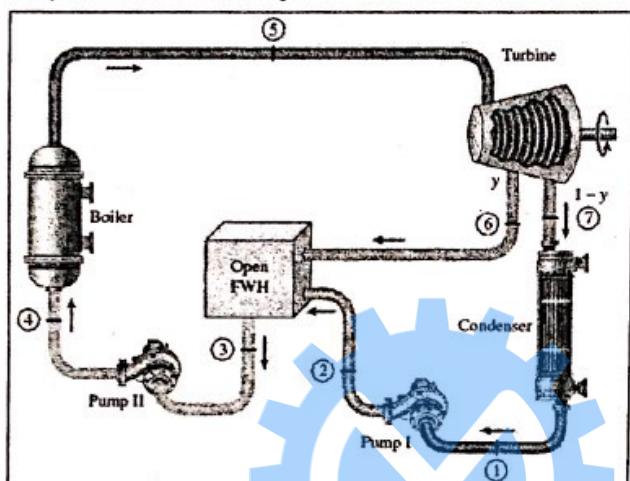
### Problem 2: (12 marks)

$$1^{\circ} = \frac{2\pi}{100}$$

A steam power plant operating on Simple Ideal Regenerative Rankine Cycle with OFWH.

The steam enters the turbine at 25 MPa and 1000K, it expands to 2 MPa where some steam is extracted to the OFWH. Then the remaining steam enters the condenser at 10 kPa, Calculate :

- 1) Quality of steam at OFWH inlet and turbine exit.
- 2) Work output of turbine and work input to the pumps.  $W_t$
- 3) Heat supplied in the boiler and lost in the condenser.  $T_{in} - T_{out}$
- 4) Mass fraction used for regeneration.
- 5) Thermal efficiency of the cycle.
- 6) Carnot efficiency.



$$\text{stated } P_1 = 1013 \text{ Pa } \quad \left. \begin{array}{l} h_1 = 191.81 \text{ kJ/kg} \\ T_1 = 1000 \text{ K} \end{array} \right\} v_f = \underline{0.00101 \text{ m}^3/\text{kg}}$$

$$\begin{aligned} \text{State 2} \quad P_2 &= 2 \text{ MPa} & h_2 &= h_1 + v_1 (P_2 - P_1) \\ S_2 &= S_1 & & = 191.81 + 0.0010 \end{aligned}$$

$$\text{State 3: } P_3 = 2 \text{ MPa} \quad h_3 = \frac{908.47 \text{ kJ/kg}}{V_3 = 0.001172 \text{ m}^3/\text{kg}} \quad \checkmark$$

$$\begin{aligned} \text{STATE 4} \\ P_4 = 26 \text{ MPa} \quad \left. \begin{aligned} h_4 = h_3 + v_3 [P_4 - P_3] \\ = 908.47 + 0.0177 [26000 - 2000] = 949.18 \text{ kJ/kg} \end{aligned} \right\} \text{WEP}_2 \quad \text{WEP}_2 \\ s_3 = s_4 \end{aligned} \quad 935.85$$

$$\text{State 5} \quad P_5 = 25 \text{ MPa} \quad \left. \begin{array}{l} h_5 = 3848.30 \text{ kJ/kg} \\ T_5 = 1000 \text{ K} \end{array} \right\} \quad \left. \begin{array}{l} S_5 = 6.7409 \text{ kJ/kg.K} \end{array} \right.$$

$$\text{State 6} \quad p_c = 2 \text{ MPa} \quad \left. \begin{array}{l} h_6 = 3009.14 \text{ kJ/kg} \\ s_6 = s_f = 6.7401 \end{array} \right\} \text{Saturated water}$$

$$s_{turb} = 7 \quad P_2 = 10 \text{ kPa} \quad s_2 = s_{fg} \quad x = \frac{s_2 - s_f}{s_{fg}} = \frac{6.7409 - 0.6492}{7.4996} = 0.8122$$

$$h_7 = h_f + x h_{f_3} \\ = 191.81 + (0.8122 \times 239.21) = 2134.6 \text{ kPa}$$

$$\dot{E}_{in} = \dot{E}_{out}$$

Ansatz

$$\gamma h_c + (1-\gamma) h_2 = h_3$$

$$\gamma = \frac{h_3 - h_2}{h_0 - h_2}$$

$$\gamma = \frac{m_0}{m_5}$$

$$\gamma = \frac{908.47 - 193.81}{3009.14 - 192.81}$$

$$\frac{m_0}{m_5} = 0.253$$

$$\underline{\underline{= 0.253}}$$

$$\underline{\underline{= 25\%}}$$

$$q_{in} = h_5 - h_4$$

$$= 3848.3 - 949.18$$

$$= \underline{\underline{2899.12 \text{ kJ/kg}}} \quad \underline{\underline{2914.5}}$$

$$q_{out} = (1-\gamma) (h_2 - h_1)$$

$$= (1 - 0.253)(2134.6 - 191.81)$$

$$= \underline{\underline{1451.26 \text{ kJ/kg}}}$$

$$W_{net} = q_{in} - q_{out}$$

$$= 2899.12 - 1451.26$$

$$= \underline{\underline{1447.8}}$$

$$\eta_{th} = 1 - \frac{q_{out}}{q_{in}} \quad \underline{\underline{1447.8 / 2899.12}}$$

$$= 1 - \frac{1451.26}{2899.12}$$

$$= 0.499 \approx \underline{\underline{49.9\%}} \approx 50\%$$

$$\eta_{th, Carnot} = 1 - \frac{T_{min}}{T_{max}}$$

$$\underline{\underline{= 1 - \frac{45.81 + 273}{1000}}}$$

$$= 1 - \frac{45.81 + 273}{1000}$$

$$= 0.6811$$

$$= \underline{\underline{68\%}} \rightarrow \underline{\underline{6.6986}}$$

## Problem 3: (8 marks)

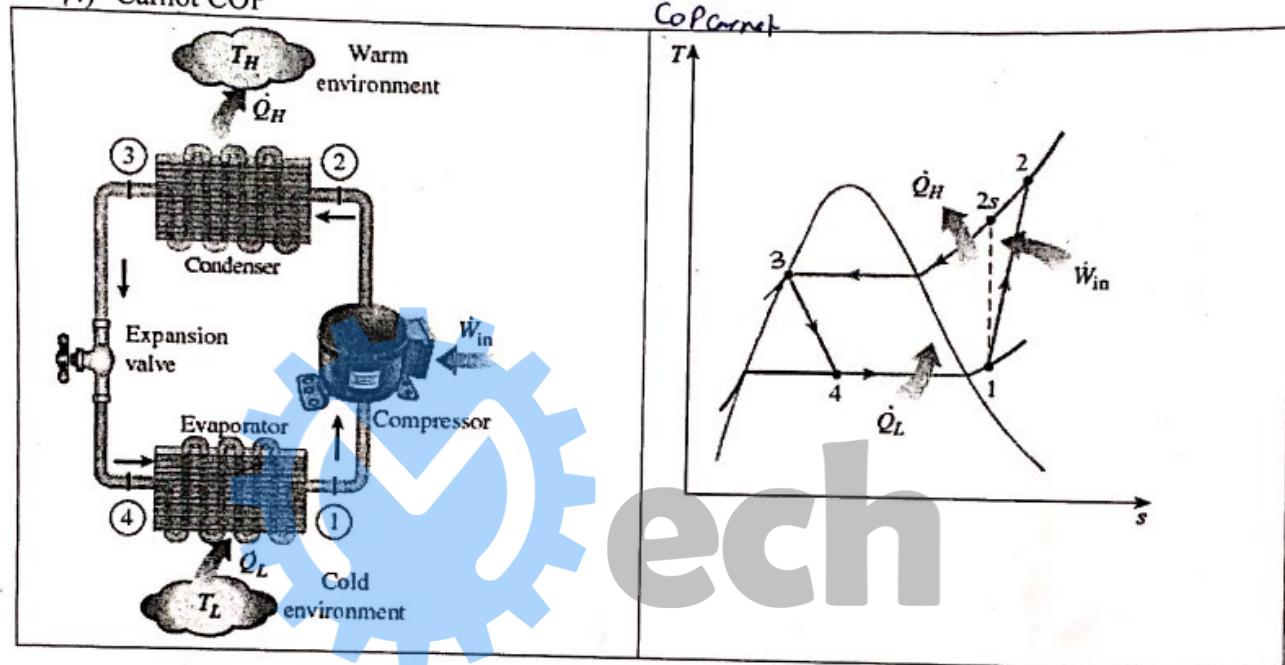
An Actual Vapor Compression Refrigeration Cycle uses refrigerant R134a to maintain a space at  $-13^{\circ}\text{C}$  by rejection heat to ambient air at  $27^{\circ}\text{C}$ . The refrigerant enters the compressor at 100kPa superheated by  $6.4^{\circ}\text{C}$  at mass flow rate of  $0.05 \text{ kg/s}$ . The isentropic efficiency of the compressor is 85%. The refrigerant leaves the condenser at  $39.4^{\circ}\text{C}$  as saturated liquid, calculate:

1) The cooling load provided by this cycle.  $Q_L$

2) The COP for the cycle.  $\text{COP}$

3) The compressor power needed for this cycle.  $Q_L$ ,  $Q_H$

4) Carnot COP



$$P_1 = 100 \text{ kPa}$$

$$\begin{aligned} T_1 &= T_{\text{Sat}} + \Delta T \\ &= -26.4 + 6.4 \\ &= -20^{\circ}\text{C} \end{aligned}$$

$$\begin{aligned} P_2 &= P_3 = 1000 \text{ kPa} \\ s_{2s} &= s_1 = 0.9721 \text{ kJ/kg.K} \end{aligned} \quad \left. \begin{aligned} h_1 &= 239.52 \text{ kJ/kg} \\ h_2s &= 289.14 \text{ kJ/kg} \end{aligned} \right.$$

$$\begin{aligned} P_3 &= 1000 \text{ kPa} \\ h_3 &= 107.34 \text{ kJ/kg} \end{aligned} \quad \left. \begin{aligned} s_3 &= 0.3919 \end{aligned} \right.$$

$$h_4 = h_3 = 107.34 \text{ kJ/kg}$$

$$\begin{aligned} P_4 &= 100 \text{ kPa} \\ h_4 &= 107.34 \text{ kJ/kg} \end{aligned} \quad \left. \begin{aligned} s_4 &= 0.4368 \text{ kJ/kg.K} \end{aligned} \right.$$

$$\gamma_c = \frac{h_{2s} - h_1}{h_2 - h_1}$$

$$0.85 = \frac{289.14 - 239.52}{h_2 - 239.52} \Rightarrow h_2 = \underline{\underline{297.9 \text{ kJ/kg}}}$$

$$\left. \begin{array}{l} P_2 = 1000 \text{ kPa} \\ h_2 = 297.9 \text{ kJ/kg} \end{array} \right\} s_2 = 0.9984 \text{ kJ/kg.K}$$

$$Q_L = m(h_1 - h_4) = 0.05 (239.52 - 107.34) = \underline{\underline{6.609 \text{ kW}}}$$

$$Q_H = m(h_2 - h_3) = 0.05 (297.9 - 107.34) = \underline{\underline{9.528 \text{ kW}}}$$

$$\dot{w}_{in} = m(h_2 - h_1) = 0.05 (297.9 - 239.52) = \underline{\underline{2.919 \text{ kW}}}$$

$$COP_R = \frac{Q_L}{\dot{w}_{in}} = \frac{6.609}{2.919} = \underline{\underline{2.264}}$$

$$COP_{R, \text{Carnot}} = \frac{T_L}{T_H - T_L} = \frac{(-13 + 273)}{[2227 - (-13)]} = \underline{\underline{6.5}}$$